

RESEARCH OF COTTON SPEED DURING PNEUMATIC CONVEYING SYSTEM

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ABSTRACT. The article considers the movement of a mixture of air and raw cotton through a pipeline with a variable cross-section as a multi-speed heterogeneous medium. The regularities of the movement of components inside the pipeline, the equation of change in the porosity of cotton, air pressure and component velocities in time and along the transportation line are obtained.

KEY WORDS: Air pressure; fiber; pipeline; porosity; pneumatic transportation; raw cotton; the mixture.

INTRODUCTION. GENERAL CONCEPTS.

Depending on the number of components in the pipeline transport, one-component and multi-component media are distinguished. A single-component medium is a medium consisting of a single material or substance, which is called a homogeneous mixture, and a multi-component – of several materials or substances that differ in physical, mechanical, chemical and other properties, which is called a heterogeneous mixture [1]. The mathematical description of the motion of a multicomponent medium is complicated by the difference in the reaction of each component to the movement of another. Therefore, to simplify the process of theoretical consideration, multicomponent media are taken as a one-component or two-component medium consisting of a continuous phase – air and a discrete phase - material, which ultimately gives more General and less accurate result [2].

Especially, when considering the processes of pneumatic transportation of materials, including raw cotton, the theory of motion of a discrete medium in a stationary or moving continuous medium has been adopted to date, which will give a more or less distorted idea of the process of moving air and material inside the pipeline. More suitable, in our opinion, to study the process of pneumatic transportation theory, is the theory of multi-speed systems, according to which, all components are moved through the pipeline separately, with interdependent parameters, including speed, which is a new approach to the study of the processes

of pneumatic transportation of materials. To ensure the universality of the laws, consider the motion of the mixture inside the pipeline with a variable cross section [3,4,5].

The mixture of air with fiber particles is assumed to be a heterogeneous mixture, to describe the motion of which you can use the theory of multi-speed systems proposed in the work of Ch.E. Rakhmatullin[6].

Heterogeneous mixtures, as a rule, are described by a multi-speed model taking into account the dynamic effects arising due to the mismatch of the speeds of the individual phases. At the same time, we consider the air to be an ideal fluid and the internal force of interaction is determined through the normal pressure, which is common to the whole mixture, opposite to the direction of movement of the particles of the fibrous medium [7,8].

2. SIMULATION OF THE MOVEMENT OF COTTON AND AIR FLOW IN A PIPELINE

Set the origin of the coordinates in the initial section of the pipeline. We direct the axis along the axis of the pipeline, the cross-sectional area of which varies according to the law, considering the process stationary, denoted by, respectively, the air velocity (index-) and cotton particles of raw mass (index-1) in an arbitrary section of the pipeline. We believe that in the cross section of the pipeline the air flow with speed acts on the moving mass of the mixture. The equations of one-dimensional motion of the components of the mixture and the laws of mass conservation, according to, are written in the form

$$\rho_0 u_0 s \frac{du_0}{dx} = -\frac{\rho_0}{\rho_0^{(0)}} \frac{d(sp)}{dx} + sk(u_1 - u_0) \quad (1)$$

$$\rho_1 u_1 s \frac{du_1}{dx} = -\frac{\rho_1}{\rho_1^{(0)}} \frac{d(sp)}{dx} - sk(u_1 - u_0) \quad (2)$$

$$\rho_0 u_0 s = u_{00} \rho_{00} s_0 = const, \quad \rho_1 u_1 s = u_{10} \rho_{10} s_0 = const, \quad \rho_0 = m \rho_0^{(0)}, \quad \rho_1 = (1-m) \rho_1^{(0)}$$

$$\rho_0 = \frac{m}{m_0} \rho_{00}, \quad \rho_1 = \frac{1-m}{1-m_0} \rho_{10} \quad (3)$$

in ρ_0, ρ_1, m - respectively, given the density of air, fibrous mass and porosity in an arbitrary section of the pipe, $\rho_0^{(0)}$ and $\rho_1^{(0)}$ - their true densities are, k - coefficient of resistance, ρ_{00}, ρ_{10} and m_0 - known values of air density, fibrous mass and porosity in cross section $x = 0$.

From (3) the following relations follow

$$u_0 = \frac{m_0}{m} \frac{s_0}{s} u_{00}, \quad u_1 = \frac{1-m_0}{1-m} \frac{s_0}{s} u_{10}, \quad \frac{\rho_0^{(0)}}{\rho_0} + \frac{\rho_1^{(0)}}{\rho_1} = 1 \quad (4)$$

Equations (1) and (2) we bring to the form

$$\rho_0^{(0)} u_0 s \frac{du_0}{dx} = -\frac{d(sp)}{dx} + \frac{\rho_0^{(0)}}{\rho_0} sk(u_1 - u_0) \quad (5)$$

$$\rho_1^{(0)} u_1 s \frac{du_1}{dx} = -\frac{d(sp)}{dx} - \frac{\rho_1^{(0)}}{\rho_1} sk(u_1 - u_0) \quad (6)$$

Excluding the derivative from the system $\frac{d(sp)}{dx}$, we get

$$\rho_0^{(0)} u_0 \frac{du_0}{dx} - \rho_1^{(0)} u_1 \frac{du_1}{dx} = \left(\frac{\rho_0^{(0)}}{\rho_0} + \frac{\rho_1^{(0)}}{\rho_1} \right) k(u_1 - u_0) \quad (7)$$

Equations (3) and (4) imply that the densities and velocities of the components in an arbitrary section of the pipeline are expressed in terms of porosity $m(x)$, which after excluding speeds $u_0(x)$, $u_1(x)$ from equation (7) with the help of relations (4), satisfies the equation:

$$\frac{dm}{dx} = \frac{F_1(m)}{F_0(m)} \frac{s'(x)}{s(x)} + \frac{F_2(m)}{F_0(m)} \frac{s_0}{s(x)} \quad (8)$$

Where:

$$F_0 = \rho_0^{(0)} u_{00}^2 m_0^3 (1-m)^3 + \rho_1^{(0)} u_{10}^2 m^3 (1-m_0)^3,$$

$$F_1 = -m(1-m) [\rho_0^{(0)} u_{00}^2 m_0^2 (1-m)^2 - \rho_1^{(0)} u_{10}^2 m^2 (1-m_0)^2],$$

$$F_2 = m^2 (1-m)^2 k [u_{00} m_0 (1-m) - u_{10} m (1-m_0)]$$

The pressure $p(x)$ is determined by the formula

$$p = \frac{s_0}{s} \left[p_0 + u_{00}^2 \rho_{00} \left(1 - \frac{m_0}{m} \frac{s_0}{s} \right) + u_{10}^2 \rho_{10} \left(1 - \frac{1-m_0}{1-m} \frac{s_0}{s} \right) \right] \quad (9)$$

where p_0 - is the pressure of the mixture in cross section $x = 0$

The densities $\rho_0(x)$, $\rho_1(x)$ and velocities of the components $u_0(x)$, $u_1(x)$ are expressed in terms of porosity by the formulas (3) and (4).

In the process of transporting the mixture on the inner wall from the side of the particles of the solid component (cotton particles of raw) acts lateral pressure $q = k_0 p$ (k_0 -coefficient of lateral pressure), which in the direction of motion creates a frictional force $f q L$ (f -coefficient of friction between the raw and the surface of the pipe, $L = l(x)$ - the length of the contour of the cross-section of the pipe), determined, for example, by the law of dry friction Kulon. In this case, equation (1) and (2) are written in the form:

$$\rho_0 u_0 s \frac{du_0}{dx} = -\frac{\rho_0}{\rho_0^{(0)}} \frac{d(sp)}{dx} + sk(u_1 - u_0) \quad (10)$$

$$\rho_1 u_1 s \frac{du_1}{dx} = -\frac{\rho_1}{\rho_1^{(0)}} \frac{d(sp)}{dx} - sk(u_1 - u_0) - k_0 l f p (1-m) \quad (11)$$

After excluding the derivative $\frac{d(sp)}{ds}$ from system (1) and (11), we obtain

$$\rho_0^{(0)} u_0 \frac{du_0}{dx} - \rho_1^{(0)} u_1 \frac{du_1}{dx} = k(u_1 - u_0) + \frac{\rho_1^{(0)}}{s\rho_1} (1-m)lk_0fp$$

After the statement of the expressions of derivatives $\frac{du_0}{dx}$ and $\frac{du_1}{dx}$ taking into account dependencies (4), we obtain

$$\frac{dm}{dx} = Z(m, x, p)$$

$$Z(m, x, p) = \frac{F_1(m)}{F_0(m)} \frac{s'(x)}{s(x)} + \frac{F_2(m)}{F_0(m)} \frac{s_0}{s(x)} - \frac{k_0 fl(x) s(x) m^3 (1-m)^3}{s_0^2} p$$

To determine the derivative $\frac{d(sp)}{ds}$ we add equations (10) and (11) and, taking into account (3), we have

$$\rho_{00} u_{00} \frac{du_0}{dx} + \rho_{10} u_{10} \frac{du_1}{dx} = -\frac{dp}{dx} - lk_0 fp(1-m)/s.$$

Adding the values of the derivatives $\frac{du_0}{dx}$ and $\frac{du_1}{dx}$ we get:

$$\frac{dp}{dx} + Z_0(m, x)p = Z_1(x, m, p) \tag{12}$$

$$\text{Here } Z_0 = \frac{l(x)k_0 f(1-m)}{s(x)}, \quad Z_1(x, m, p) = F_3(x, m, p) + F_4(x, m),$$

$$F_3 = \frac{s_0^2}{s^2(x)} \frac{Z(x, m, p)}{m^2(1-m)^2} [\rho_{00} u_{00}^2 m_0^2 (1-m) - \rho_{10} u_{10}^2 (1-m_0)^2 m],$$

$$F_4 = \frac{s_0^2}{s^2(x)} \frac{s'(x)}{s(x)} \frac{1}{m(1-m)} [\rho_{00} u_{00}^2 m_0 (1-m) + \rho_{10} u_{10}^2 m(1-m_0)]$$

Equations (11) and (12) together describe a system that satisfies the following initial conditions for determining cotton porosity and pressure:

$$\text{at } x=0 \quad m = m_0, \quad p = p_0 = \rho_{00} u_{00}^2 / 2.$$

3. ANALYSIS OF THE MOTION OF A TWO-COMPONENT MEDIUM

The equations are processed by the Maple 2015 program with the following parameters for a constant-section pipeline and the corresponding graphical dependencies are obtained: $m_0 = 0.4$, $u_{00} = 20m/s$, $\rho_{00} = 1.2\kappa z / m^3$, $Q_0 = 10000\kappa z / hour$, $\rho_{10} = 38\kappa z / m^3$, $s = s_0 = \pi D^2 / 4$, $l = \pi D$, $k_0 = 0.6$. The current coefficient of porosity of cotton is equal $m = 0.6$, and the boundary values of the coefficient of interaction are respectively equal $k_n = 50Hc / m^4$, $k_n = 100Hc / m^4$, $k_n = 200Hc / m^4$, $k_n = 300Hc / m^4$ [9,10].

In Figures 1–4 present the results of an analysis of the equations for the diameter of the pipeline $D = 0.4\text{m}$: the change in the porosity of the cotton $m(x)$, the velocity of the component $u_0(x)$, $u_1(x)$, and the pressure $p(x)$ along the length of the pipeline.

To establish the influence of the friction coefficient f on the transportation process, the calculations were made for its various values. In the absence of friction, the movement of the transported material occurs at all values of the interaction coefficient large from zero ($k > 0$). And, in the presence of friction, the movement occurs at $k \geq k_n$, (k_n -boundary value of the coefficient. At smaller values of this coefficient k . At smaller values of this coefficient ($k < k_n$) in some sections of the pipeline, the pressure breaks down and movement will not occur. For such cases, the adopted model does not work. For all other cases, the equations obtained correctly describe the process of moving a two-phase flow.

For example, with $f = 0.05$, $f = 0.1$, $f = 0.2$ and $f = 0.3$, the interaction coefficient will have the following values: $k_n = 8.7Hc / \text{m}^4$, $k_n = 16.8Hc / \text{m}^4$, $k_n = 35.4Hc / \text{m}^4$, $k_n = 50.5Hc / \text{m}^4$.

The analysis shows that the value of porosity (Fig. 1), retains the property of a regular total increase for large values k_n (the graph on the right) is relatively smaller (the graph on the left) and is about 0.85. At the same time, when $k = 400Hc / \text{m}^4$ the increase is much more intense at the beginning of the process, and after passing through 24-25 meters, it remains relatively constant.

On the pressure graph (Fig. 2) there is a difference with the initial parameters - the pressure at the beginning of the pipeline is about 75 Pa for smaller (graph on the left), 95 Pa (graph on the right) for larger values k_n . However, the pressure value at lower values k_n in the initial 1-2 meters of the pipeline decreases sharply. When reaching 20 meters the intensity drops, then the pressure is relatively stabilized. At high values k_n , the pressure decreases with almost the same intensity.

The graph of air velocity (Fig. 3) shows the property of decline with the same intensity for all values k_n . When it reaches 50 m, the air velocity drops to 14-12 m / s, then almost does not change. And the speed of cotton (Fig. 4), starting from the 0th value, gradually increases. And when it reaches 50 m, it is relatively stabilized with a value of 7-8 m / s.

Then, it remains almost unchanged, and the speed of cotton (Fig. 4), on the contrary, is of increasing nature. If you look at the charts, the speed of the cotton in the initial 20 meters of the pipeline length changes dramatically, then more stably.

At large values of the interaction coefficient, although at the beginning of the pipeline the speed changes greatly, after passing about 30 m distance there is no significant change in speed.

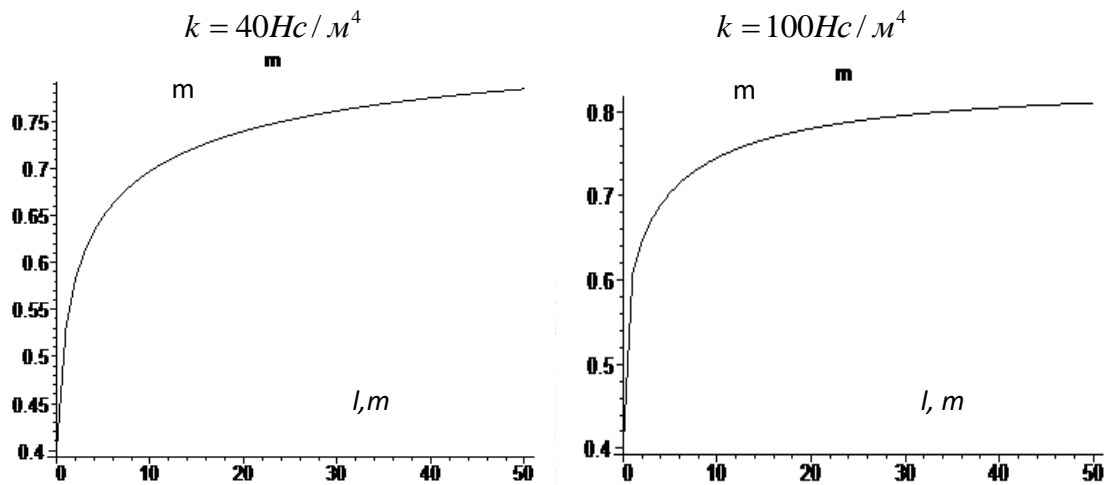


Fig.1. Changing the porosity of cotton along the length of the pipeline

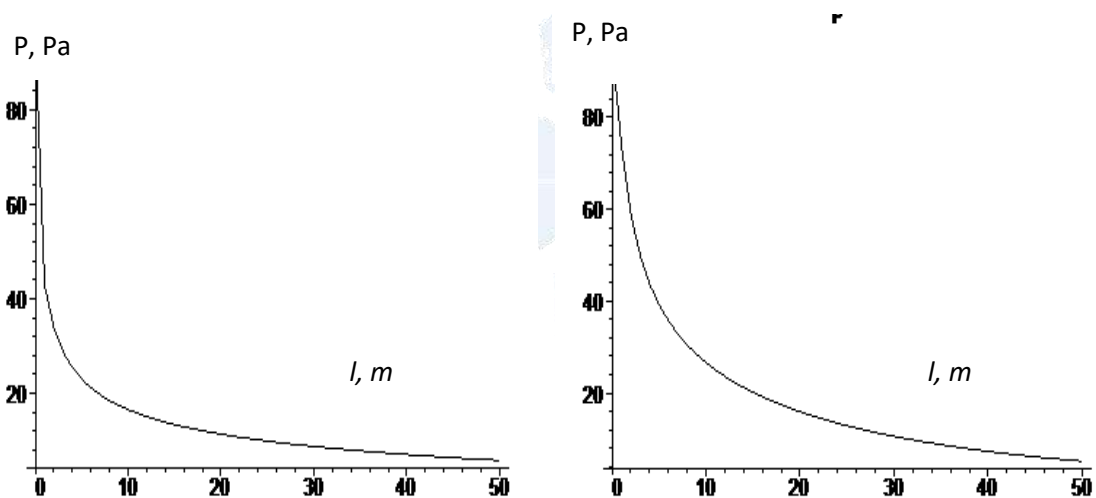


Fig.2. The change in air pressure along the length of the pipeline

At large values of the interaction coefficient, the nature of the change of parameters is preserved. The difference is only the intensity of the change. Figure 5 represents the change in the porosity of cotton in both cases at a distance of 50m reaches the same value, 0.75-0.80.

Only with a large k , the growth of porosity in the initial 10–20 meters is much stronger and when it reaches 30 m, the change is significantly stabilized. As the change in pressure, on the contrary (Fig. 6), with smaller k decreases more strongly than relatively large k . This shows that k negatively affects the resistance force, i.e., with its increase, the resistance force decreases, and with decreasing, on the contrary, it increases.

In both cases (Fig. 7) and values, the air velocity shows a character of decline with almost the same intensity. Only if in the first graphs the stabilization of air

velocity occurs at a value of 9-10 m / s, then in the following graphs, i.e., at large values, the air velocity remains without changes after the value of 15 m / s.

The speed of cotton (Fig. 8) also changes according to the previous pattern: at smaller values k_n the intensity of the increase in speed is relatively low, but this increase is maintained for a long time, and at large values k_n the growth rate is much higher, but after 30 meters the speed of cotton is almost stabilized. At the same time, the speed is about 9-10 m / s. If you pay attention to the air speed, you can see its value - at a distance of 40 - 50 meters it is about 14 - 15 m / s, that is, the air is ahead of cotton with a relative speed equal to the difference of their speeds. The ratio of cotton velocity to air velocity will give the latency coefficient, which in our case is equal to the tabular values of $k = 0.7 - 0.75$ [8]. This ratio shows how late cotton is from air. The fact of the equality of theoretical values with the table values, which are established experimentally, proves the compliance of the established theoretical pattern with the natural pattern of movement of the cotton-air mixture in the transport pipelines of pneumatic installations and will provide an opportunity to offer the established formulas for the calculation of pneumatic transport and its design.

The resulting model is universal and can be used for calculations of pipelines with variable cross-section.

Conclusions.

(1) Research has established that during pneumatic transportation, in the initial 20–25 meters of the pipeline, the porosity of transported cotton greatly increases, which indicates that its exposure to tensile deformation and proves that cotton is loosened, fluffed, and trash is separated from it.

(2) The entry of cotton into the pneumatic conveying pipeline leads to a sharp decrease in pressure and air velocity, and the speed of cotton in the initial 15 to 20 meters of the pipeline increases strongly, then with more moderate intensity.

(3) The multi-speed model of the movement of a cotton-air mixture as a heterogeneous medium in pneumotransport pipelines more correctly describes the process of moving air and material during pneumatic transportation, which makes it possible to suggest its use for calculating pneumatic transport and in its design.

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